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Determination of grindability characteristics of zeolite

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Abstract. In this study grindability of zeolite was studied. The work index of zeolite was determined for three different test sieves. In terms of work indexes, there was insignificant difference between the test sieves. Additionally, the breakage rate and distribution parameters were also determined. The fastest breakage rate was obtained for -1700+1180 μm feed sizes and found breakage distributions functions were non-normalisable.

keywords: Bond work index, zeolite, breakage rate function, breakage distribution function, ball milling

1. Introduction

Zeolites are crystalline aluminosilicates of the alkaline and alkaline earth minerals. Zeolites are widely used in mineral industries such as animal nutrition, detergent, pozzolanic cement and agricultural products (Englert and Rubio, 2005). They possess many desirable properties (ion exchange, molecular sieving, catalytic etc.) which make them valuable mineral commodities (Clifton, 1987). In recent years, natural zeolites, especially clinoptilolite (CLN), are gaining growing interest in environmental application such as ammonium and heavy metal removal from wastewater. They are readily available from several producers, less expensive than synthetic counter parts and have advantages of high selectivity towards the ammonium ions removal from wastewater.

Grinding is an important industrial operation that is used for size reduction of materials, production of large surface area and liberation of valuable minerals from their matrices. As it is known, a significant amount of energy, which is used in grinding, turns into heat energy and cannot be used in grinding effectively. However, it is possible to obtain a more effective grinding by setting up more effective grinding systems which consume less energy (Ipek et.al, 2004). Increased rates and efficiencies of milling have been sought through the optimization of milling by providing favorable physical and operational conditions for the mills used (Ozkan et.al, 2009).

Therefore, the design and scale-up of ball mills are important issues in size reduction processes.

The objective of this study is to determine the grindability characteristics of zeolite and to investigate the effect of feed particle size upon grinding.

2. Theoretical background

The Bond ball mill grindability test gives the Bond ball mill work index. This index expresses the resistance of a material to ball milling since the higher the value of the Bond ball mill work index, the more difficult it is to grind the material using a ball mill. This index is widely used in the mineral industry for comparing the resistance of different material to ball milling, estimating the energy required for ball milling and scaling-up ball mill (Man, 2002). Test results were converted to a work index (in kWh/Mg) by the following empirical equation:

$$W_i = \frac{48.95}{P_t^{0.23} G^{0.82} \left[\frac{10}{P_{80}^{0.5}} - \frac{10}{F_{80}^{0.5}} \right]}, \text{ kWh/Mg} \quad (1)$$

where: P_t is selected test size (μm); G is net mass (grams) of undersize product per unit revolution of the mill, in g/rev; P_{80} is the 80% passing product particle size (μm); F_{80} the 80% passing feed particle size (μm).

The value of W_i obtained by above equation is representative of the required energy to tumble the charge of a 30.5 cm interior diameter overflow ball mill dry grinding in a closed circuit. Estimation of W_i is realized only after attainment of steady-state conditions for a locked-cycle batch grinding test. A grinding cycle consists of the following two parts:

- dry grinding of 700 cm³ bulk volume of material prepared to -3350 micrometers in a 30.5 by 30.5 cm ball mill rotating at 70 rpm and charged with 22,648 grams of grinding balls. Balls plus ore charge is ground for desired revolutions which is usually 50 or 100 revolutions,
- removal by sieving the portion of the product which was ground finer than a pre-selected test size, P_t . In preparation for the next cycle, the undersize portion is replaced by an equivalent amount of fresh feed in order to maintain constant charge.

The duration of grinding is established as the time required to produce, for the next cycle, a simulated 250% re-circulating load of particles coarser than the selected test size. An estimate of the grinding time is obtained using the grindability, G , of the previous cycle. G is defined as the grams of particles finer than test size produced per mill revolution. An initial value of G is obtained by waiving the 250% re-circulating load requirement for the first cycle and replacing it with a grind period of 100 mill revolutions. When G reverses its direction and remains constant from cycle to cycle, steady-state grinding conditions are said to prevail. The average value of G for the final three cycles is taken as G , the steady, state grindability (McIntyre and Plitt, 1980, Deister, 1987).

Selection of the test size, P_t , is usually based on the fineness of grind desired in the milling operation. Typical choices for P_t are 106, 75 and 53 micrometers. Care must be taken to minimize the possibility of sieve blinding. Blinding will cause underestimation of G , with direct consequences on the calculate value of W_i . (Bond, 1961)

In the analysis of the breakage materials, it is useful to make the initial assumption that the breakage of each size fraction is first order in nature. The rate of disappearance of size 1 due to breakage is proportional to the amount of size 1 material in the mill holdup (Yan and Eaton, 1994):

$$-\frac{d[w_1(t)W]}{dt} \propto w_1(t)W \tag{2}$$

Since the mill hold up, W , is constant, this becomes:

$$dw_1(t)/dt = -S_1 w_1(t) \tag{3}$$

where S_1 is a proportionality constant and it is called the specific rate of breakage, with units of time^{-1} . If S_1 does not vary with time (Austin et al., 1984)

$$w_1(t) = w_1(0) \exp(-S_1 t) \tag{4}$$

that is,

$$\log[w_1(t)] = \log[w_1(0)] - S_1 t / 2.3 \tag{5}$$

where $w_1(t)$ is the weight fraction of mill hold up that is of size 1 at time t (Austin and Bagga, 1981). The formula proposed by Austin et al. (1984) for the variation of the specific rate of breakage S_i with particle size is

$$S_i = a_T \left(\frac{x_i}{x_0} \right)^\alpha Q_i \tag{6}$$

where x_i is the upper limits of the size interval indexed by i , x_0 is 1 mm, a_T and α are model parameters that depend on the properties of the material and the grinding conditions. Q_i is a correction factor which is 1 for smaller sizes (normal breakage) and less than 1 (abnormal breakage) for particles too large to be nipped and fractured properly by the ball size in the mill. In abnormal breakage region, each size behaves as if it has some fraction of weak material and the remaining fraction of stronger material. Using a mean value for S_i in this region, values of Q_i are empirically described by

$$Q_i = \frac{1}{1 + (x_i/\mu)^\Lambda}, \Lambda \geq 0 \tag{7}$$

where μ is the particle size at which correction factor is 0.5 and Λ a positive number which an index of how rapidly the rates of breakage fall as size increases that is the higher the value of Λ , the more rapidly the values decrease.

The Cumulative Breakage Distribution, $B_{i,j}$, is defined as “the weight fraction of material broken from size j which falls less than the upper size of size interval i ” is commonly used to characterize the size distribution resulting from breakage of

material from a particular size interval to a smaller size (Austin et al., 1984, Austin and Luckie, 1971/72).

The values of the primary breakage distribution function are deduced from the size distributions at short grinding times where there is mainly size 1 material breaking and only a small amount of smaller sizes to rebreak (Austin et al., 1984). B values can be calculated by using BII method which is described following formula:

$$B_{i,j} = \frac{\log [(1 - P_i(0))] / \log [(1 - P_i(t))]}{\log [(1 - P_{j+1}(0))] / \log [(1 - P_{j+1}(t))]} \quad (8)$$

where j is the top size of the charge, $P_i(t)$ is the cumulative percent undersize of size interval i at the short grinding time which gives no more than about 30% broken out of the top size interval. Cumulative primary breakage distribution function $B_{i,j}$ is also defined in an empirical form by

$$B_{i,j} = \phi_j \left(\frac{x_{i-1}}{x_j} \right)^\gamma + (1 - \phi_j) \left(\frac{x_{i-1}}{x_j} \right)^\beta \quad (9)$$

where x_i is the top size and $B_{i,j}$ is the weight fraction of primary breakage products. The parameters Φ , γ and β define the size distribution of the material being ground. On plotting size versus $B_{i,j}$ on the log scale, the slope of the lower portion of the curve gives the value of γ while the slope of the upper portion of the curve gives the value of β , and Φ is the intercept as shown in Fig. 1.

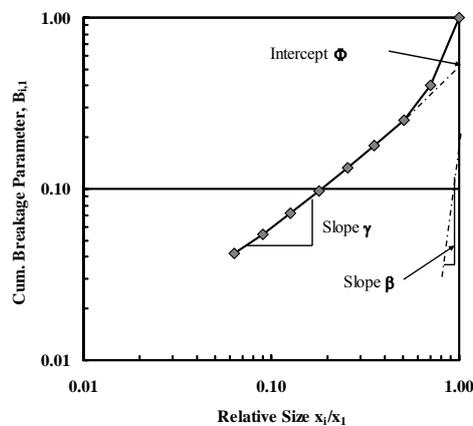


Fig. 1. Obtaining primary breakage distribution function parameters for any single size fraction feed ground in the mill

The primary characteristic of the B_{ij} curves is the final slope of each plot γ . The smaller the curve of γ , the higher the relative amounts of progeny fines that are produced from breakage. Conversely, materials having a large γ value give less relative amounts of fines and can therefore be expected to produce steeper size distributions when ground in a given machine. The β , and Φ values show how rapidly

fractions close to feed size are reduced to a lower size. The $B_{i,j}$ values are said to be normalisable if the fraction which appears at sizes less than the starting size is independent of the starting size. In terms of plots, the curves should be super-imposed on each other if the $B_{i,j}$ values are normalisable. If the values of breakage distribution are dependent on starting feed size, that is, if they are normalisable, the $B_{i,j}$ values are represented by the following equation (Austin et al., 1984, Austin and Bagga, 1981, Austin and Luckie, 1971/72):

$$B_{i,j} = \Phi_j \left(\frac{x_{i,1}}{x_1} \right)^\gamma + (1 - \Phi_j) \left(\frac{x_{i-1}}{x_1} \right)^\beta, \quad 0 \leq \Phi_j \leq 1 \quad (10)$$

$$\Phi_j = \Phi_1 \left[\frac{x_j}{x_1} \right]^{-\delta} \quad (11)$$

for normalized B values $\delta=0$.

3. Materials and experimental methods

3.1. Material

The zeolite sample was taken from Bigadic Boron Works, Balikesir/Turkey. The sample contains zeolite group minerals (heulandite-clinoptilolite) and amorphous materials (www.etimaden.gov.tr). The chemical analysis of sample is given in Table 1.

The sample was crushed to $-3350 \mu\text{m}$ by a laboratory jaw crusher for Bond test. In order to determine the breakage parameters, crushed material of $-3350 \mu\text{m}$ was classified into seven mono size fractions which were $-3350+2360$, $-2360+1700$, $-1700+1180$, $-1180+850$, $-850+600$, $-600+425$, $-425+300 \mu\text{m}$, where for example $-3350+2360 \mu\text{m}$ denotes that 100 % of the particles are passing by weight at $3350 \mu\text{m}$ size and 100 % of particles are remaining at $2360 \mu\text{m}$. The density of zeolite sample which was determined by a pycnometer and it was averaged 2.07 g/cm^3 over thirteen measurements. Mohr's hardness of sample was measured by hardness pens and it was found to be 3.5-4.

Table 1. Chemical composition of materials

SiO ₂	Al ₂ O ₃	Fe ₂ O ₃	TiO ₂	CaO	MgO	Na ₂ O	K ₂ O	L O I	B in acid	B in water
(%)	(%)	(%)	(%)	(%)	(%)	(ppm)	(%)	(%)	(ppm)	(ppm)
70.14	11.46	0.85	0.097	2.98	1.46	354	4.37	9.50	131.13	8.00

3.2. Experimental

The stainless steel Bond mill used in the experiments was 30.5 cm in diameter and 30.5 cm in length. The mill was loaded with 22,648 g of 38.1, 31.75, 25.40, 19.05 and 12.70 mm diameters of stainless steel balls which correspond to 22% of the struck

volume of the mill and mill was operated at 70 rpm which was 86% of its critical speed.

In Bond test experiment, the mill was loaded to 32.6% of the interstitial void volume of the ball charge and was filled with the -3350 microns of sample. Test was done in the three different test sieves.

In the kinetic tests, the mill was loaded to 100% of the interstitial void volume of the ball charge, U . The breakage parameters were determined experimentally using one size fraction technique (Austin and Bagga, 1981). Tests were carried out for 7 different mono size fractions which were mentioned above. In order to obtain the breakage parameters, the mono size fractions were ground dry for 0.5, 1.0, 2.0, 4.0, 8.0 minutes separately. At the end of the each run, the ground product was weighed and the loss was no more than 0.15% of the total charge. Due to grinding, sampling, sieving and regrinding the same sample for several times, some weight losses are expected. The loss in this study was less than 1 % which is acceptable.

The characteristics of the Bond mill used in grinding tests and test conditions are outlined in Table 2.

Table 2. Bond mill characteristic and test conditions for grinding of zeolite

Mill	Diameter, D , cm	30.5				
	Length, L , cm	30.5				
	Volume, V , cm ³	22,272				
	Speed, rpm	70				
	Critical speed, N_c^a	86.55				
Mill charge	Diameter, d , mm	38.10	31.75	25.40	19.05	12.70
	Number	43	67	10	71	94
	Total mass, g	22,648				
	Specific gravity g/cm ³	7.79				
	Fractional ball filling, J^b	0.22				
Media charge	Sample	Zeolite				
	Specific gravity g/cm ³	2.07				
	Powder weight, g	2489.56				
	Fractional. Powder filling, f_c^c	0.09				
	Powder-ball loading ratio, U^d	1.00				

$$^a N_c = \frac{42.3}{\sqrt{D-d}},$$

$$^b J = \left(\frac{\text{mass of balls} / \text{ball density}}{\text{mill volume}} \right) \times \frac{1.0}{0.6},$$

$$^c f_c = \left(\frac{\text{mass of powder} / \text{powder density}}{\text{mill volume}} \right) \times \frac{1.0}{0.6}$$

$$^d U = \frac{f_c}{0.4J}.$$

4. Results and Discussion

4.1. Bond Work Index

Bond work tests were done in three different test sieves which were 300, 212 and 150 micrometers. The average size distribution of feed and products were given in Fig 2. Bond work indexes were 10.55, 10.71, 10.18 kWh/t respectively for this zeolite sample. Fig 3 shows the test sieve sizes versus work index values. These results are very close to each other which is unusual situation. Generally, it is expected that, the less the test sieve sizes, the higher the work index. Therefore, all tests were repeated 3 times and the difference was not more than 2%. In literature, similar results were observed for galena by Smith and Lee in 1968 (Smith and Lee, 1968).

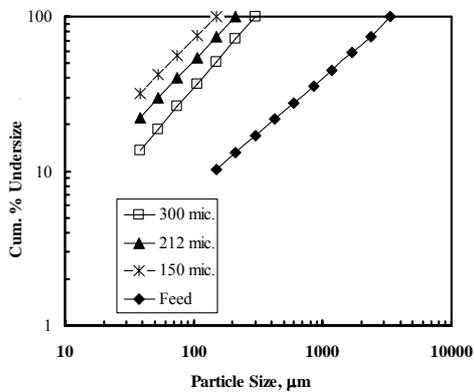


Fig. 2. Size distribution of feed and products of zeolite

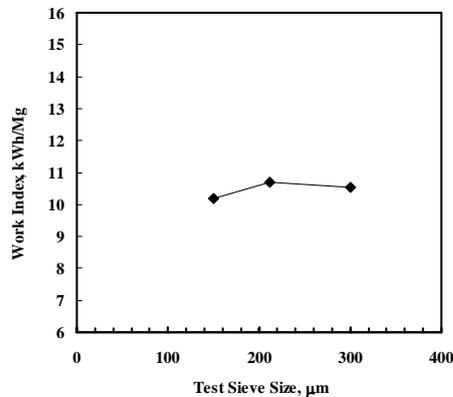


Fig. 3. Test sieve sizes versus work index values

4.2. Determination of the breakage rate function

Figure 4 shows the initial grinding results of sample plotted in first-order form for varying feed size fractions. Samples were ground individually as batch-wise for 0.5, 1.0, 2.0, 4.0, and 8.0 minutes to obtain both the breakage parameters and particle size distributions. It can be seen that, all feed size fractions match first-order rate kinetics. Coefficients of correlation are between 0.9989 to 0.9863.

Variation of the specific rates of breakage (S_i) with particle size of the sample is shown in Fig. 5. It is clearly seen that S_i values increase up to a maximum particle size then started to decrease at 1700 μm . This was due to the inefficiency of the largest feed sizes that were not nipped properly in the mill.

The initial grinding results obey the first-order breakage form as in Eq. (6). When the values of S_i are fitted to the expression (6), the a_T value is obtained by inserting α , x_i and x_0 . Using Eq.(6), S_i , a_T , α , μ and λ parameters were obtained and outlined in Table 3 as the breakage parameters that were utilized in the simulations.

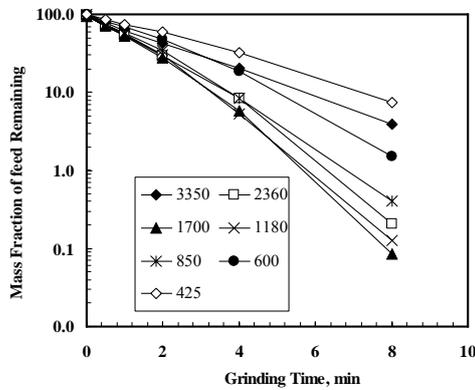


Fig. 4. First order plots for dry grinding of different feed sizes of zeolite

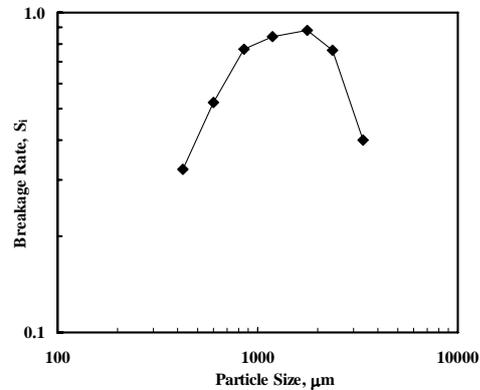


Fig. 5. Variation of the S_i values zeolite with particle size

Table 3. The overall breakage parameters for zeolite sample

a_T	α	μ	Λ	Φ	γ	β	δ
0.98	1.23	1.65	3.10	0.44	1.09	2.52	0.16

4.3. Determination of the primary breakage distribution function

The values of $B_{i,j}$ were determined from the size distributions at short grinding times using the BII method (Eq. 8). The primary breakage distribution function variations at different particle feed sizes are shown in Fig 6. The primary breakage distribution parameters were determined as indicated in Fig. 1 and results are listed in Table 4.

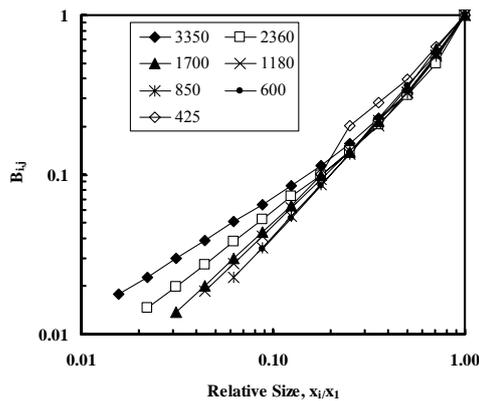


Fig. 6. Primary breakage distribution functions of zeolite

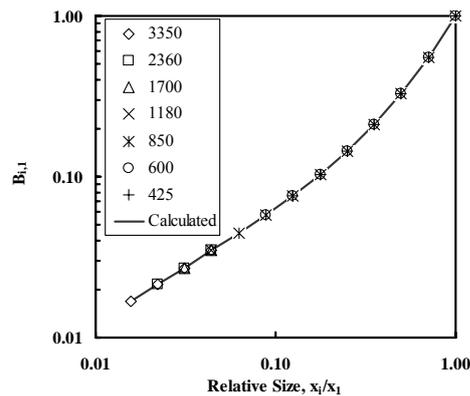


Fig. 7. Normalized primary breakage distribution functions of zeolite

Figure 6 and Table 4 show that, the primary breakage distribution functions were dependent on feed size. In order to normalize breakage distribution parameters, nonlinear regression technique was used to obtain the sum of the square of differences between the measured and calculated breakage distribution values. In this calculation, Eq. 11 was used instead of ϕ in Eq. 10. These parameters (ϕ , γ , β , δ) are listed in Table 3 and normalized breakage distribution functions are shown in Fig.7. This figure shows that calculated and experimental data were in good agreements.

Table 4. The primary breakage distribution parameters obtained from short grinding times

Particle Size (μm)	Φ	γ	β
-3350+2360	0.47	0.80	2.71
-2360+1700	0.53	0.95	3.10
-1700+1180	0.68	1.13	2.27
-1180+850	0.69	1.16	2.95
-850+600	0.80	1.29	3.69
-600+425	0.92	1.37	7.73
-425+300	0.94	1.36	2.29

5. Conclusion

No significant differences in the Bond work index test were found for three different test sieves. That means that the work index values of zeolite was independent of test sieve sizes. The grinding of zeolite obeys the first order breakage kinetics in the case of all feed sizes. Faster breakage (represented by α parameters) from higher values to lower values were at -1700+1180 micrometers fraction. Different $B_{i,j}$ values (ϕ , β and γ) were obtained for each feed size fractions. It was seen that the breakage distributions obtained by the BII method were dependent on all starting feed sizes and this could not be normalized. When all model parameters were used, it was determined that all sizes were in conformity with all laboratory grinding data. The breakage parameters, obtained from the laboratory size mill, could be used for scaling up the industrial mills. This is performed by choosing the scale-up option in the simulation program for the mineral studied.

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